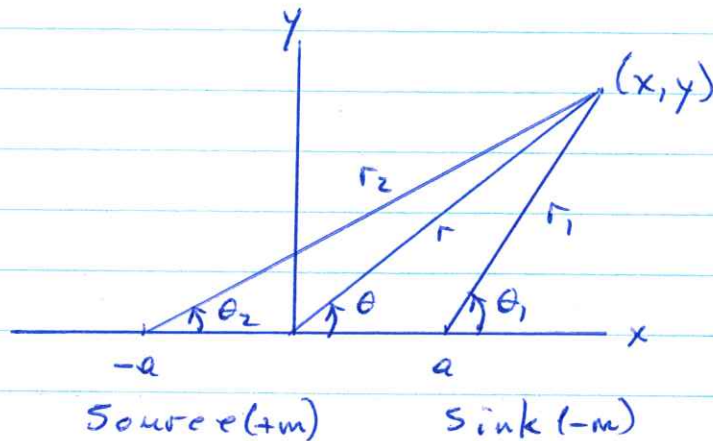


Assignment 5

1. Doublet = source at $-a$ + sink at $+a$.



Total Stream Fct. $\psi = \frac{m}{2\pi} \theta_2 - \frac{m}{2\pi} \theta_1$

$$\begin{aligned} \text{Now } \tan \theta_1 &= \frac{y}{x-a} & + \tan \theta_2 &= \frac{y}{x+a} \\ &= \frac{r \sin \theta}{r \cos \theta - a} & &= \frac{r \sin \theta}{r \cos \theta + a} \end{aligned}$$

$$\tan \theta_2 - \tan \theta_1 = r \sin \theta \left(\frac{1}{r \cos \theta + a} - \frac{1}{r \cos \theta - a} \right)$$

$$\frac{\sin \theta_2}{\cos \theta_2} - \frac{\sin \theta_1}{\cos \theta_1} = \frac{-2ar \sin \theta}{r^2 \cos^2 \theta + a^2}$$

$$\frac{\sin(\theta_2 - \theta_1)}{\cos \theta_1 \cos \theta_2} = \frac{-2ar \sin \theta}{r^2 \cos^2 \theta + a^2}$$

$$\sin(\theta_2 - \theta_1) = \frac{-2ar \sin \theta}{r^2 \cos^2 \theta + a^2} \cos \theta_1 \cos \theta_2$$

We now take dipole limit.

$$\lim_{\substack{a \rightarrow 0 \\ m \rightarrow \infty \\ am \rightarrow \pi K}} m \sin(\theta_2 - \theta_1) = \lim_{\substack{a \rightarrow 0 \\ m \rightarrow \infty \\ am \rightarrow \pi K}} \frac{-2amr \sin \theta \cos \theta_1 \cos \theta_2}{r^2 \cos^2 \theta + a^2}$$

$$= \lim_{\substack{a \rightarrow 0 \\ am \rightarrow \pi K}} \frac{-2\pi K r \sin \theta \cos^2 \theta}{r^2 \cos^2 \theta}$$

$$= -\frac{2\pi K \sin \theta}{r}$$

$$\text{For } \theta_2 - \theta_1 \text{ small } \Rightarrow m(\theta_2 - \theta_1) = \frac{-2\pi K \sin \theta}{r}$$

$$\therefore \text{stream fct. } \psi = \frac{-K \sin \theta}{r}$$

2a) Exam notes: $\psi = U r \sin \theta + \frac{m \theta}{2\pi}$

Velocity: $v_r = U \cos \theta + \frac{m}{2\pi r}$

$$v_\theta = -U \sin \theta$$

Stagnation point by symmetry occurs on $-x$ axis.

\therefore set $v_r(\theta = \pi) = 0$

$$-U + \frac{m}{2\pi r} = 0$$

$$r = \frac{m}{2\pi U} \equiv +b.$$

\therefore stagnation point occurs at $x = -b = -\frac{m}{2\pi U}$.

b) $\psi(x = -b) = \psi(\theta = \pi, r = b)$

$$= U b \sin \pi + \frac{m \pi}{2\pi}$$

$$= \frac{m}{2}$$

c) $\psi = \frac{m}{2} \Rightarrow \frac{m}{2} = U r \sin \theta + \frac{m \theta}{2\pi}$

$$\frac{m}{2} = U y + \frac{m \theta}{2\pi}$$

$$U y = \frac{m}{2\pi} (\pi - \theta)$$

$$y = b (\pi - \theta)$$

d) Bernoulli Equ. along streamline ($z = \text{const.}$)
gives:

$$P_0 + \frac{1}{2} \rho U^2 = P + \frac{1}{2} \rho v^2$$

$$\text{Now } v^2 = v_r^2 + v_\theta^2$$

$$= \left(U \cos \theta + \frac{m}{2\pi r} \right)^2 + (-U \sin \theta)^2$$

$$= U^2 \left(1 + \frac{2b \cos \theta}{r} + \frac{b^2}{r^2} \right)$$

$$\therefore P = P_0 - \frac{\rho U^2}{2} \left(\frac{2b \cos \theta}{r} + \frac{b^2}{r^2} \right)$$

3. In notes, we showed steady flow between 2 plates gives:

$$P = -\rho g y + f_1(x)$$

$$u = \frac{1}{2\mu} \frac{dP}{dx} y^2 + c_1 y + c_2$$

Couette flow: $u(y=0) \Rightarrow c_2 = 0$

$$u(y=b) = U \Rightarrow U = \frac{1}{2\mu} \frac{dP}{dx} b^2 + c_1 b$$

$$c_1 = \frac{1}{b} \left[U - \frac{1}{2\mu} \frac{dP}{dx} b^2 \right]$$

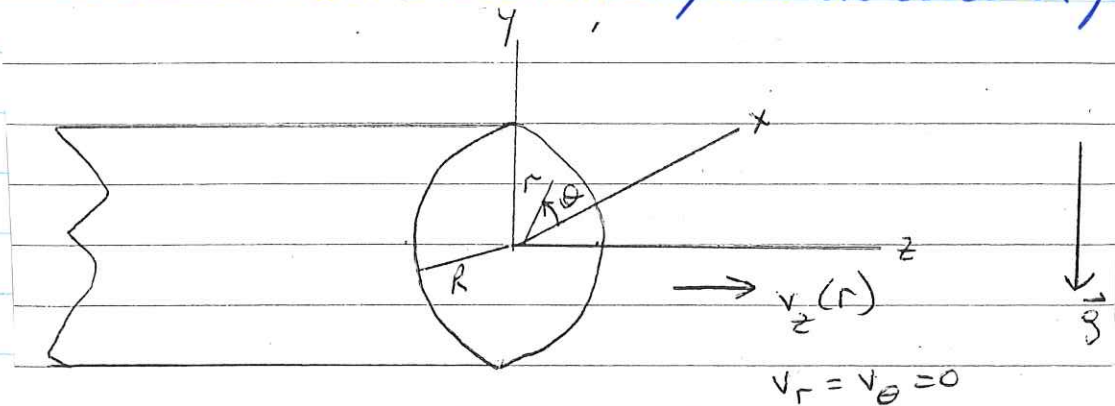
$$\therefore u = \frac{1}{2\mu} \frac{dP}{dx} y^2 + \frac{1}{b} \left[U - \frac{1}{2\mu} \frac{dP}{dx} b^2 \right] y$$

$$= \frac{y}{b} U + \frac{1}{2\mu} \frac{dP}{dx} \left[y^2 - \frac{y}{b} b^2 \right]$$

$$\frac{u}{U} = \frac{y}{b} - \frac{b^2}{2\mu U} \frac{dP}{dx} \left[\frac{y}{b} - \frac{y^2}{b^2} \right]$$

$$\frac{u}{U} = \frac{y}{b} + P' \frac{y}{b} \left(1 - \frac{y}{b} \right) \text{ where } P' \equiv -\frac{b^2}{2\mu U} \frac{dP}{dx}$$

4. Poiseuille Flow: laminar flow in circular pipe



Velocity

$$v_z = v_z(r)$$

$$v_r = v_\theta = 0$$

a) Substituting \vec{v} into Navier Stokes equations for steady flow gives:

$$0 = -\rho g \sin \theta - \frac{\partial P}{\partial r} \quad (1)$$

$$0 = -\rho g \cos \theta - \frac{1}{r} \frac{\partial P}{\partial \theta} \quad (2)$$

$$0 = -\frac{\partial P}{\partial z} + \frac{\mu}{r} \frac{\partial}{\partial r} \left(r \frac{\partial v_z}{\partial r} \right) \quad (3)$$

b) (1) + (2) $\Rightarrow P = -\rho g r \sin \theta + f_1(z)$

$\therefore \frac{\partial P}{\partial z}$ is independent of $\theta + r$.

$$(3) \Rightarrow \frac{\partial P}{\partial z} = \frac{\mu}{r} \frac{\partial}{\partial r} \left(r \frac{\partial v_z}{\partial r} \right)$$

$$\frac{r^2}{2\mu} \frac{\partial P}{\partial z} = r \frac{\partial v_z}{\partial r} + K_1$$

$$\frac{r}{2\mu} \frac{dP}{dz} = \frac{dv_z}{dr} + \frac{K_1}{r}$$

$$\frac{r^2}{4\mu} \frac{dP}{dz} = v_z + K_1 \ln r + K_2$$

But v_z is well defined at $r=0 \Rightarrow K_1=0$.

$$\therefore v_z = \frac{r^2}{4\mu} \frac{dP}{dz} - K_2$$

$$\text{But } v_z(r=R)=0 \Rightarrow v_z = \frac{1}{4\mu} \frac{dP}{dz} (r^2 - R^2)$$

c) Volume Flow rate $Q = \int_0^R v_z 2\pi r dr$

$$= \frac{1}{4\mu} \frac{dP}{dz} 2\pi \int_0^R (r^2 - R^2) r dr$$

$$Q = -\frac{\pi}{8\mu} \frac{dP}{dz} R^4$$